

Electrocatalytic Reaction of $\text{Fe}^{2+/3+}$ Aqua Ions by $[\text{Mo}(\text{CN})_8]^{4-/3-}$ Complexes

Keiichi SATO,[†] Takeo OHSAKA, Hiroaki MATSUDA,[†] and Noboru OYAMA*

Department of Applied Chemistry for Resources, Tokyo University of Agriculture and Technology, Koganei, Tokyo 184

[†]Department of Electronic Chemistry, Tokyo Institute of Technology, Midori-ku, Yokohama 227

(Received January 24, 1983)

Synopsis. The catalysis of the oxidation of Fe^{2+} aqua ion by $[\text{Mo}(\text{CN})_8]^{3-}$ ion, which is formed on an electrode surface, and that of the reduction of Fe^{3+} aqua ion by $[\text{Mo}(\text{CN})_8]^{4-}$ ion were examined by means of hydrodynamic voltammetry at a rotating disk pyrolytic graphite electrode. The rate constants of the electron transfer cross-reaction of the $\text{Fe}^{2+}/[\text{Mo}(\text{CN})_8]^{3-}$ and $\text{Fe}^{3+}/[\text{Mo}(\text{CN})_8]^{4-}$ systems were estimated to be $(7.0 \pm 0.5) \times 10^6$ and $(6.6 \pm 0.5) \times 10^6 \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$, respectively.

In previous papers^{1,2)} we have examined the catalysis of the electrode process of $\text{Fe}^{2+/3+}$ redox couple by $[\text{Mo}(\text{CN})_8]^{4-/3-}$ complexes bound electrostatically to graphite electrodes coated with the protonated poly(4-vinylpyridine) (PVP) film. It has been shown therein that $[\text{Mo}(\text{CN})_8]^{4-/3-}$ complexes are strongly incorporated into the protonated PVP film and the resulting metalated film electrode can catalyze both the oxidation of Fe^{2+} aqua ion and the reduction of Fe^{3+} aqua ion present in a bulk solution. The catalytic reaction of the $\text{Fe}^{2+}/[\text{Mo}(\text{CN})_8]^{3-}$ and $\text{Fe}^{3+}/[\text{Mo}(\text{CN})_8]^{4-}$ systems can be considered to be simple and outer-sphere electron transfer cross-reaction. However, no kinetic study on the catalytic reaction of both systems in a bulk solution at an uncoated electrode has been reported yet.

In this paper, we will thus examine the catalysis of the oxidation of Fe^{2+} ion by $[\text{Mo}(\text{CN})_8]^{3-}$ ion, which is formed on a graphite electrode surface, and that of the reduction of Fe^{3+} ion by $[\text{Mo}(\text{CN})_8]^{4-}$ ion by means of hydrodynamic voltammetry at a rotating disk pyrolytic graphite electrode.

Experimental

Electrochemical apparatus and the experimental procedures have been described previously.^{1–3,8)} The exposed area of each electrode was 0.17 cm^2 . Potassium octacyanomolybdate(IV) dihydrate ($\text{K}_4[\text{Mo}(\text{CN})_8] \cdot 2\text{H}_2\text{O}$) was synthesized according to the standard procedure.⁴⁾ Solutions were freed of air with prepurified argon prior to the electrochemical measurements. Experiments were conducted at 25°C . Potentials are reported with respect to a sodium chloride saturated calomel electrode (SSCE).

Results and Discussion

Current-potential curves A, B, and C shown in Fig. 1 demonstrate typical steady-state current-potential curves obtained at a rotating disk graphite electrode in an each $0.2 \text{ M CF}_3\text{COONa}$ solution containing $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{4-}$, 2 mM Fe^{2+} and $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{4-} + 2 \text{ mM Fe}^{2+}$ ions. When the current-potential curves were measured at a graphite electrode in the solution containing both $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{4-}$ and 2 mM Fe^{2+} ions, two waves were observed and each of their half-wave potentials were about 0.5 and 0.7 V vs. SSCE . The first wave observed at about 0.5 V corresponds to the oxidation of $[\text{Mo}(\text{CN})_8]^{4-}$ ion. The conventional log-plot of $\log \{i/(i - i_{\text{lim}})\}$ against E (where i_{lim} is the limiting current and i is the current at any potential,

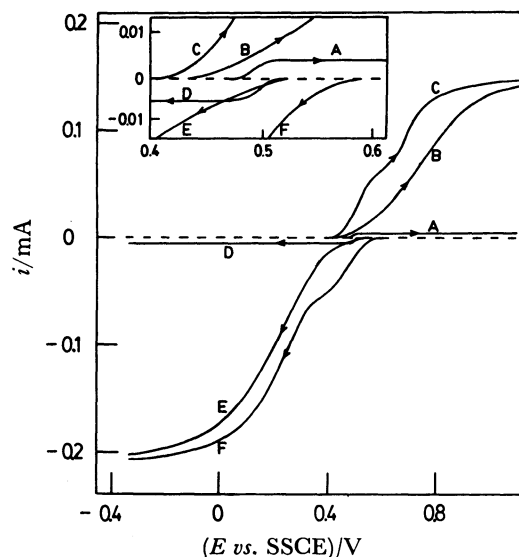


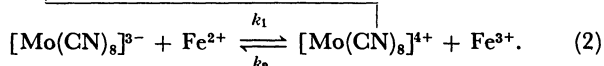
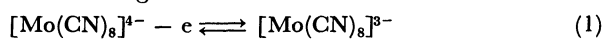
Fig. 1. Typical steady-state current-potential curves demonstrating the catalysis of the oxidation of Fe^{2+} ion by $[\text{Mo}(\text{CN})_8]^{3-}$ ion and of the reduction of Fe^{3+} ion by $[\text{Mo}(\text{CN})_8]^{4-}$ ion at rotating disk pyrolytic graphite electrodes.

Oxidation of (A): $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{4-}$; (B): 2 mM Fe^{2+} ; (C): $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{4-} + 2 \text{ mM Fe}^{2+}$; Reduction of (D): $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{3-}$; (E): 2 mM Fe^{3+} ; (F): $0.2 \text{ mM } [\text{Mo}(\text{CN})_8]^{3-} + 2 \text{ mM Fe}^{3+}$.

Supporting electrolyte: $0.2 \text{ M CF}_3\text{COONa}-\text{CF}_3\text{COOH}$ (pH 1.5). Electrode rotation rate: 800 min^{-1} .

E) of the current-potential curve A yields straight lines with the reciprocal slopes of $59 \pm 1 \text{ mV}$, in accordance with the fact that the first wave is the reversible one-electron oxidation wave. From the similar log-plot of the current-potential curve B, the oxidation of Fe^{2+} ion was proved to be close to irreversible. The standard heterogeneous rate constant for the oxidation of Fe^{2+} ion at a graphite electrode is $6 \times 10^{-5} \text{ cm s}^{-1}$.⁸⁾ As can readily be seen from the comparison of the limiting currents of the steady-state current-potential curves A and C shown in Fig. 1, the limiting current for the oxidation of $[\text{Mo}(\text{CN})_8]^{4-}$ ion in the solution containing Fe^{2+} ion is several times larger than the corresponding limiting current in the absence of Fe^{2+} ion. As the concentration of Fe^{2+} ion increased under the constant concentration of $[\text{Mo}(\text{CN})_8]^{4-}$ ion, the height of the first wave increased, but the half-wave potential at about 0.5 V remained constant. At the constant concentrations of Fe^{2+} and $[\text{Mo}(\text{CN})_8]^{4-}$ ions, the height of the first wave unchanged with changes in the rotation rate between 400 and 3600 min^{-1} , but the total limiting current was proportional to the square root of the rotation rate. These facts suggest the catalytic oxidation of Fe^{2+} ion by $[\text{Mo}(\text{CN})_8]^{3-}$ ion, which is formed on an electrode surface by the electrochemical oxidation of the $[\text{Mo}(\text{CN})_8]^{4-}$ ion present in a bulk solution.

Thus, the overall electrode reaction can be expressed by the following scheme:



Under the conditions that the concentration of Fe^{2+} ion is so high compared with that of $[\text{Mo}(\text{CN})_8]^{4-}$ ion, it can be assumed that the concentration Fe^{2+} ion remains constant during the whole electrochemical process. Thus, we obtain Eq. 3 which characterizes the catalytic current, i_{cat} , of the reaction process expressed by Eqs. 1 and 2, together with the conditions expressed by Eq. 5 which must be fulfilled to maintain the validity of Eq. 3.^{5,6)}

$$\frac{i_{\text{cat}}}{i_L} = \frac{\sqrt{\lambda}}{\tanh \sqrt{\lambda}} \quad (3)$$

with

$$\lambda = (1 + K)k_1 C_{\text{Fe}^{2+}} \delta^2 / D \quad (4)$$

and

$$\frac{C_{\text{Fe}^{2+}}}{C_{[\text{Mo}(\text{CN})_8]^{3-}}} \gg \frac{i_{\text{cat}}}{i_L} \quad (5)$$

where i_L is the Levich current⁵⁾ for the oxidation of $[\text{Mo}(\text{CN})_8]^{4-}$ ion, k_1 and k_2 are the forward and backward rate constants of reaction 2, respectively, the equilibrium constant, K , is k_2/k_1 , $C_{[\text{Mo}(\text{CN})_8]^{3-}}$ and $C_{\text{Fe}^{2+}}$ denote the concentrations of $[\text{Mo}(\text{CN})_8]^{3-}$ and Fe^{2+} ions, respectively, D is the common value of the diffusion coefficients of $[\text{Mo}(\text{CN})_8]^{4-}$ and $[\text{Mo}(\text{CN})_8]^{3-}$ ions and δ is the steady-state thickness of the diffusion layer ($\delta = 1.62 D^{1/3} \nu^{1/6} \omega^{-1/2}$, ν : the kinematic viscosity, ω : the electrode rotation rate).

Figure 2 shows the plots of the ratio i_{cat}/i_L against the inverse square root of the electrode rotation rate at the various concentrations of Fe^{2+} and $[\text{Mo}(\text{CN})_8]^{4-}$ ions, together with the similar plots for the $\text{Fe}^{3+}/[\text{Mo}(\text{CN})_8]^{4-}$ system. The value of k_1 was evaluated by curve fitting method and estimated to be $(7.0 \pm 0.5) \times 10^6 \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$ by using $\nu = 1 \times 10^{-2} \text{ cm}^2 \text{ s}^{-1}$,⁷⁾ $K = 4.7$ (calculated using the standard redox potentials,¹⁾ i.e., 0.49 and 0.53 V vs. SSCE for $\text{Fe}^{2+}/\text{Fe}^{3+}$ and $[\text{Mo}(\text{CN})_8]^{4-}/[\text{Mo}(\text{CN})_8]^{3-}$ couples, respectively) and $D = 5.0 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$. The value of D was the average value of the diffusion coefficients for $[\text{Mo}(\text{CN})_8]^{4-}$ and $[\text{Mo}(\text{CN})_8]^{3-}$ ions obtained from the limiting currents of the steady-state current-potential curves by using the Levich equation.⁵⁾ The solid lines shown in Fig. 2 represent the best fit curves calculated by using Eq. 3, which are seen to reproduce the experimental results. As can easily be seen from Fig. 2, the plots of i_{cat}/i_L vs. $\omega^{-1/2}$ give the straight lines whose slopes are proportional to the square root of the concentration of Fe^{2+} ion, indicating that in this case the r.h.s. of Eq. 3 can be reduced to $\sqrt{\lambda}$, i.e., $\tanh \sqrt{\lambda} \approx 1$, as can be expected for a fast catalytic reaction. By introducing the obtained value of k_1 and other known values of D , ν , ω and $C_{\text{Fe}^{2+}}$ into the right-hand side of the inequality (Eq. 5), it was confirmed that this inequality is fulfilled under the experimental conditions employed.

From the current-potential curves E and F shown in

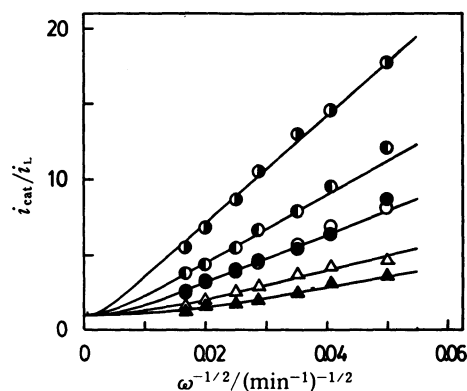


Fig. 2. Plot of the ratio, i_{cat}/i_L , against the inverse square root of the rotation rate, $\omega^{-1/2}$.

○: 0.2 mM $[\text{Mo}(\text{CN})_8]^{4-}$ + 2 mM Fe^{2+} ; ●: 0.2 mM $[\text{Mo}(\text{CN})_8]^{4-}$ + 4 mM Fe^{2+} ; ○: 0.2 mM $[\text{Mo}(\text{CN})_8]^{4-}$ + 10 mM Fe^{2+} ; ●: 0.05 mM $[\text{Mo}(\text{CN})_8]^{4-}$ + 2 mM Fe^{2+} ; ▲: 0.2 mM $[\text{Mo}(\text{CN})_8]^{3-}$ + 2 mM Fe^{3+} ; △: 0.2 mM $[\text{Mo}(\text{CN})_8]^{3-}$ + 4 mM Fe^{3+} .

Supporting electrolyte and scan rate of electrode potential are the same as in Fig. 1. Solid lines are the best fit curves calculated by Eq. 3.

Fig. 1, it is also apparent that the reduction of Fe^{3+} ion present in a bulk solution is catalyzed by the $[\text{Mo}(\text{CN})_8]^{4-}$ ion formed on a graphite electrode surface. By means of the same method as described above, the rate constant (k_2) of the electron transfer cross-reaction between Fe^{3+} and $[\text{Mo}(\text{CN})_8]^{4-}$ ions was estimated to be $(6.6 \pm 0.5) \times 10^6 \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$.

The values of k_1 and k_2 are by 1 to 2 orders of magnitude larger than those ($k_1 = 3.8 \times 10^5$ and $k_2 = 1.0 \times 10^4 \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$) reported in a previous paper,²⁾ where the $[\text{Mo}(\text{CN})_8]^{4-}$ or $[\text{Mo}(\text{CN})_8]^{3-}$ ion was bound electrostatically to the protonated poly(4-vinylpyridine) (PVP) film on a graphite electrode and Fe^{2+} or Fe^{3+} ion was present in a bulk solution. The similar results have been previously reported in the case of the catalysis of the oxidation of Fe^{2+} ion by the $[\text{IrCl}_6]^{2-}$ ion bound to the protonated PVP film on an electrode or present in a bulk solution.⁸⁾ This may be mainly attributed to the differences in the reaction media in which the rate constants were measured.

References

- 1) N. Oyama, K. Sato, and H. Matsuda, *J. Electroanal. Chem.*, **115**, 149 (1980).
- 2) N. Oyama, N. Ohta, Y. Ohnuki, K. Sato, and H. Matsuda, *Nippon Kagaku Kaishi*, **1983**, 940.
- 3) N. Oyama, S. Yamaguchi, Y. Nishiki, K. Tokuda, H. Matsuda, and F. C. Anson, *J. Electroanal. Chem.*, **139**, 371 (1982).
- 4) N. H. Furman and C. O. Miller, *Inorg. Syn.*, **3**, 160 (1950).
- 5) Z. Galus, "Fundamentals of Electrochemical Analysis," Translation Ed.: G. F. Reynolds, John Wiley and Sons Inc., New York, London, Sydney, Toronto (1976).
- 6) J. M. Hale, *J. Electroanal. Chem.*, **8**, 332 (1964).
- 7) A. J. Bard and L. R. Faulkner, "Electrochemical Methods," John Wiley and Sons, New York, Chichester, Brisbane, Toronto (1980), Chap. 8.
- 8) N. Oyama and F. C. Anson, *Anal. Chem.*, **52**, 1192 (1980).